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**Edinburgh**  
**EH2 3NS**  
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- Patents ADP number (if you know it) **8322919002** **19SEP02 E749390-1 002866**  
**P01/7700 0.00-0221712.3**
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4. Title of the invention **METHODS OF TREATMENT**
5. Name of your agent (if you have one) **ERIC POTTER CLARKSON**  
**PARK VIEW HOUSE**  
**58 THE ROPEWALK**  
**NOTTINGHAM**  
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## METHODS OF TREATMENT

This invention relates to induction or augmentation of labour during parturition.

5

The induction of labour was applied in 18% of all U.S. deliveries in recent years (Stubbs, 2000, *Clin Obstet Gynecol* 43, 489-94). One reason for the application of this technique is that perinatal mortality increases in pregnancies over 42 weeks, but can be reduced by the induction of labour  
10 (Alfirevic Z and Walkinshaw SA, 1994, *Br J Hosp Med* 52,218-21).

15

Most commonly, oxytocin and prostaglandins and synthetic prostaglandin are used to induce labour. Intravenous prostaglandin E2 and F2 alpha can be used to induce labour by ripening of the cervix. However, their use is associated with higher rates of maternal side effects and uterine hyperstimulation than oxytocin (Luckas M, Bricker L, 2000, *Cochrane Database Syst Rev* 4, CD002864).

20

Oxytocin is a neurohypophyseal peptide hormone that induces labour and lactation in mammals (Yuan *et al*, 2002 *J Med Chem* 45, 2512-2519). Oxytocin is the commonest labour induction agent used worldwide (Kelly and Tan, 2001, *Cochrane Database Syst Rev*, 3, CD003246).

25

Oxytocin (OT) binds to specific receptors of myometrial cells, inducing and increasing myometrial contractions. During pregnancy and especially close to term, an increase in the myometrial OT-receptor concentration is found, leading to an increased sensitivity of the myometrium towards circulating OT. The factors determining the receptor level are not completely understood, but may include the level of steroids, OT- and oestrogen  
30 receptors. Because of the increased sensitivity, only a small increase in the

maternal OT blood-level is necessary to induce myometrial contractions at term. The level of maternal plasma OT does not change significantly throughout pregnancy. The fetus is found to secrete considerable amounts of OT during the first stage of labour, which reaches the myometrium in spite of the high level of oxytocinase in placenta. At the second stage of labour the distension of the lower birth canal might cause release of OT from the maternal neurohypophysis into the blood, increasing the myometrial contractions. This mechanism is observed in animals, but not established in the human (Giraldi *et al*, 1990, *Dan Med Bull*, 37, 377-83).

10

For the induction and augmentation of labour, oxytocin is presently administered by slow intravenous infusion preferably by means of an infusion pump. Once labour is progressing, oxytocin infusion may be gradually withdrawn.

15

Oxytocin has also been given, as the citrate, in the form of a buccal tablet to induce labour; however, absorption is irregular following buccal administration and this route has been superseded by intravenous administration.

20

A first aspect of the invention provides an effervescent formulation comprising oxytocin. It may be used for the induction or augmentation of labour.

25 By 'effervescent formulation' we mean that the formulation is effervescent when placed in an aqueous solution.

By 'oxytocin' we include a cyclic nonapeptide having the structure of the hormone produced by the posterior lobe of the pituitary that stimulates the contraction of the uterus: it has the structure Cys-Tyr-Ile-Gln-Asn-Cys-

30

Pro-Leu-Gly-NH<sub>2</sub> cyclic (1→6) disulphide; [2-leucine, 7-isoleucine]vasopressin; has a CAS registry number 50-56-6 and is also called alpha-hypophamine and oxytocinum. Also included are salts thereof, including acetate and citrate.

5

Effervescent formulations offer an advantage over the existing forms of supplying oxytocin as they have a high level of patient acceptability. Effervescent formulations also give a more consistent pharmacokinetic profile than buccal delivery. The formulations may be placed on the tongue  
10 where they effervesce, and release the oxytocin.

A preferred embodiment of the invention is that the effervescent formulation comprises multilayer effervescent microspheres. The manufacture of certain suitable multilayer effervescent microspheres is  
15 described in WO 98/31342 and US Patent No 6,210,711 B1, hereby incorporated by reference in their entirety.

A still further embodiment of the invention is that the multilayer effervescent microspheres contain an acidic substance, a basic substance  
20 and water-soluble isolating agent.

The term 'microsphere' will be intended to refer to microgranules formed of a support material consisting of a matrix in which the oxytocin is dispersed. In accordance with the European Pharmacopoeia monograph on spheres,  
25 microspheres have an average diameter of less than 1.0 mm and greater than or equal to 1.0 µm. They are generally intended for oral or parenteral administration and are used either as constituents of pharmaceutical form, such as tablets, or in their natural form combined or otherwise with other excipients, and distributed or otherwise in unit doses, such as sachets, gel-  
30 capsules or powder for injectable preparation.

The 'water-soluble isolating agent' may be any such agent which serves as both a binder and as an isolating barrier intended to avoid an effervescent reaction between the alkaline substance and the acidic substance during the preparation process but also during storage of the microspheres, irrespective of the storage conditions. Typically, it is chosen from polyvinylpyrrolidone, hydroxypropyl cellulose, methyl cellulose, lactose and sucrose.

By 'acidic substance' we include a powder of acidic nature containing an organic acid, for example citric acid, ascorbic acid or acetylleucine.

By 'basic substance' we mean a powder of alkaline nature containing a sodium bicarbonate or any other carbonate usually used in the preparation of effervescent forms, such as lithium hydrogen carbonate, monosodium carbonate, lithium glycine carbonate, monopotassium carbonate, calcium carbonate or magnesium carbonate. It is preferred that the 'basic substance' is a sodium salt such as sodium bicarbonate.

A preferred embodiment of the invention relates to multilayer effervescent microspheres containing an acidic substance, a basic substance and a water-soluble isolating agent whose dissolution in water leads, after almost immediate effervescence, to a solution or a homogeneous dispersion of oxytocin.

25

According to a first variant of this embodiment of the invention, the water-soluble isolating agent is dispersed in the entire bulk of each microsphere, the latter having a two-layer structure: a layer of acidic substance in which is dispersed the water-soluble isolating agent and a layer of alkaline substance in which is dispersed the water-soluble isolating agent.

30

According to a second variant of this embodiment of the invention, the water-soluble isolating agent is in the form of a thin film separating the acidic and alkaline substances. In this case, each microsphere has a three-  
5 layer structure: a layer of acidic substance and a layer of alkaline substance separated by a layer of water-soluble isolating agent.

Whether the microspheres have a two-layer or three-layer structure, the water-soluble isolating agent serves two purposes; it acts as a binder and as  
10 an isolating barrier intended to avoid an effervescence reaction between the alkaline substance and the acidic substance during the preparation process but also during storage of the microspheres, irrespective of the storage conditions.

15 In a preferred embodiment of the invention the effervescent formulation contains oxytocin present in a unit dose amount of from about 50 ng to 100 µg such as 50 ng, 100 ng, 200 ng, 340 ng, 500 ng, 750 ng, 1 µg, 2 µg, 3 µg, 4 µg, 5 µg, 6 µg, 7 µg, 8 µg, 9 µg, 10 µg, 11 µg, 15 µg, 20 µg, 30 µg, 50 µg, 75 µg or 100 µg. Most preferably the oxytocin is present in a unit  
20 dosage amount of about 340 ng to about 11 µg.

In a further embodiment the effervescent formulation of the invention is presented in a tablet form. Methods of forming tablets suitable for the invention from such an effervescent formulation are well known to those  
25 skilled in the art. Methods of forming tablets suitable for the invention from such an effervescent formulation are well known to those skilled in the art. A tablet may be made by compression or moulding, optionally with one or more accessory ingredients. Compressed tablets may be prepared by compressing in a suitable machine the active ingredient in a free-flowing  
30 form such as a powder or granules. Moulded tablets may be made by



moulding in a suitable machine a mixture of the powdered compound moistened with an inert liquid diluent.

5 In a further embodiment the effervescent formulation of the invention is presented in a powder form. Methods of forming powders suitable for the invention from such an effervescent formulation are well known to those skilled in the art.

10 A further aspect of the invention is a process for making an effervescent formulation containing oxytocin.

15 A preferred embodiment of the invention is a process wherein the effervescent formulation comprises multilayer effervescent microspheres containing an acidic substance, a basic substance, and a water-soluble isolating agent which upon dissolution in water leads, after almost immediate effervescence, to a solution or a homogeneous dispersion of oxytocin.

20 In a further preferred embodiment of the process of the invention the acidic and/or basic substances contains or contain oxytocin.

In a further preferred embodiment of the process of the invention the process employs the method of rotary granulation in a fluidized air bed.

25 The advantage of rotary granulation applied to these effervescent compositions is the continuous linking of the operations in one and the same chamber which, as a result of the components used and certain precautions taken, induces no effervescence. Furthermore, this rotary granulation technique allows the relative proportions of the various compounds to be

modified, in particular the relative molar proportions of the acidic and basic fractions.

Specifically, the process according to the invention makes it possible  
5 advantageously to obtain effervescent forms whose relative proportion of alkaline and acidic fractions is less than the stoichiometric proportion implemented in the prior art for effervescent tablets manufactured by the granulation method, without the quality of the effervescence being adversely affected.

10

In particular, the relative proportion of the basic and acidic substances implemented in the context of the process according to the invention is less than 0.6, in particular less than 0.25.

15 All the steps of the process according to the invention are carried out under atmospheric pressure, without any specific dehydration system or any specific precautions.

The apparatus used to carry out the process for preparing the effervescent  
20 microspheres is, for example, apparatus constructed by the company Glatt, onto which a rotor tank is fitted.

Such an item of apparatus is described in patent EP 0,505,319, which we include, by way of reference, in the present application.

25

Also subject of the present invention is, firstly, a process for preparing effervescent microspheres which have a two-layer structure according to the first variant described above.

- Said process is performed by rotary granulation in a fluidized air bed combined with a system for spraying powder and a system for the tangential spraying of wetting liquid. The process comprises two continuous steps, a first step of spheronization of microspheres using a powder A and a second
- 5 step of spheronization of a powder B on the microspheres of powder A, one of the powders A and B being acidic and the other alkaline and it being possible for each of them to contain or consist of oxytocin. It is preferred that powders A or B contain but do not consist of oxytocin.
- 10 During the first spheronization, the powder A is placed in the moving rotary granulation tank and suspended in the air bed. The components of the powder A are mixed together for five minutes and the air inlet temperature is stabilised to a temperature  $T_0$ .
- 15 The powder A thus blended is sprayed with a wetting liquid containing the water-soluble isolating agent. The microspheres of powder A obtained are dried by bringing the air inlet temperature to  $T_s$  and are then optionally screened using a 1000  $\mu\text{m}$  screen. During the second spheronization, the air inlet temperature is brought to  $T_0$ . The powder B and the wetting liquid
- 20 containing the water-soluble isolating agent are then simultaneously sprayed onto the dried powder A microspheres obtained previously. The powder B is sprayed by means of the powder spraying system installed on the Glatt apparatus. The two-layer microspheres obtained are dried by bringing the air inlet temperature to  $T_s$ . After drying, the microspheres must be
- 25 packaged quickly, but a small amount of moisture uptake does not harm the storage.

During the two spheronizations, the wetting liquid containing the water-soluble isolating agent is the same, for example polyvinylpyrrolidone (PVP)

dissolved in an alcohol or an aqueous-alcoholic mixture, in particular PVP dissolved to 4% by weight in ethanol at 60% by volume.

5 The two-layer microspheres obtained according to the process of the invention have an average particle size of between 20 and 500  $\mu\text{m}$ .

A subject of the present invention is also a process for preparing effervescent microspheres which have a three-layer structure according to the second variant described above.

10

Said process is performed according to the method of rotary granulation in a fluidized air bed combined with a system for the tangential spraying of wetting liquid.

15 The process comprises three continuous steps, a first step of spheronization of microspheres using a powder A, a second step of spheronization of a water-soluble isolating agent on the microspheres of powder A, and then a third step of spheronization of a powder B on the microspheres A protected with a film of water-soluble isolating agent, one of the powders A and B  
20 being acidic and the other alkaline and it being possible for each of them to contain or consist of oxytocin. It is preferred that powders A or B contain but do not consist of oxytocin.

During the first spheronization, the powder A containing an added binder,  
25 for example PVP, is placed in the moving tank and suspended in the air bed. The components of the powder A are mixed together for five minutes and the air inlet temperature is stabilized to  $T_0$ . The powder A thus blended is sprayed with a wetting liquid. The microspheres of powder A obtained are dried by bringing the air inlet temperature to  $T_s$ . During the second  
30 spheronization, the air inlet temperature is brought to  $T_0$ . The water-soluble

isolating agent is added directly to the tank and the wetting liquid sprayed until microspheres of powder A which are coated with a film of water-soluble isolating agent are obtained, and are dried by bringing the air inlet temperature to  $T_s$ . After drying, the coated microspheres are screened and  
5 the powder B is then added directly to the rotary granulation tank when the air inlet temperature has stabilized at  $T_0$ . The three-layer microspheres are obtained by spraying the preceding microspheres with a wetting liquid. The three-layer microspheres obtained are dried by bringing the air inlet temperature to  $T_s$ . After drying, the microspheres must be packaged  
10 quickly, but a small amount of moisture uptake does not harm the storage.

During the first two steps, the wetting liquid is, for example, an aqueous-alcoholic solution, in particular ethanol at 60% by volume. During the final step, the water-soluble isolating agent can be introduced by means of the  
15 powder B, in which case the wetting liquid used will be the same as during the first two steps, or alternatively the isolating agent is introduced by means of the wetting liquid, which will be an alcoholic or aqueous-alcoholic solution containing the isolating agent, for example PVP dissolved to 4% by weight in ethanol at 60% by volume.

20

The three-layer microspheres obtained according to the process of the invention have an average particle size of between 200 and 1000  $\mu\text{m}$ .

According to the process for manufacturing microspheres, whether they are  
25 two-layer or three-layer microspheres, the powder of alkaline nature contains a sodium bicarbonate or any other carbonate usually used in the preparation of effervescent forms, such as lithium hydrogen carbonate, monosodium carbonate, lithium glycine carbonate, monopotassium carbonate, calcium carbonate, magnesium carbonate and, optionally  
30 oxytocin; whereas the powder of acidic nature contains an organic acid, for

example citric acid, ascorbic acid, acetylleucine and, optionally, oxytocin. It is preferred that the powder of alkaline nature and the powder of acidic nature contain but do not consist of oxytocin.

- 5 In a further embodiment of the process of the invention the acidic and alkaline powders can also contain a diluent, for example lactose or Glucidex; flavorings and sweeteners, for example orange flavoring, citric acid, sodium saccharinate; various excipients.
- 10 In a preferred embodiment of the process of the invention oxytocin is present such that the resulting effervescent formulation contains oxytocin present in a unit dose amount of from between 50 ng to 100 µg such as 50 ng, 100 ng, 200 ng, 340 ng, 500 ng, 750 ng, 1 µg, 2 µg, 3 µg, 4 µg, 5 µg, 6 µg, 7 µg, 8 µg, 9 µg, 10 µg, 11 µg, 15 µg, 20 µg, 30 µg, 50 µg, 75 µg or 15 100 µg. Most preferably the oxytocin is present in a unit dosage amount of 340 ng to 11 µg.

In a further embodiment of the process of the invention the effervescent formulation of the invention is presented in a tablet form. Methods of 20 forming tablets suitable for the invention from such an effervescent formulation are well known to those skilled in the art as described above.

According to one embodiment of the invention, the powder A is of alkaline nature and the powder B is of acidic nature.

25

According to another embodiment of the invention, the powder B is of alkaline nature and the powder A of acidic nature.

The wetting liquid is sprayed by means of a nozzle 1.2 mm in diameter, at 30 an average flow rate of between 10 and 30 g/min. The air inlet temperature

of the fluidized bed is between 55 and 65°C during the spheronization steps ( $T_0$ ) and between 75 and 85°C during the drying phases ( $T_s$ ).

5 The microspheres obtained according to the process of the invention contain 5 to 75% of alkaline substance, 10 to 75% of acidic substance, 3 to 15% of water-soluble isolating agent, 5 to 50% of diluent and 1 to 30% of flavorings and sweeteners and contain an appropriate amount of oxytocin such as 0.00003% to 0.02%.

10 The relative humidity of the microspheres obtained according to the process of the invention, measured for fifteen minutes by the infrared balance method at 90°C, is between 1 and 2% at the rotary granulation tank outlet.

15 The overall yield for the process is calculated from the fraction of particles smaller than 2500  $\mu\text{m}$  in size, the working yield of the spheres corresponds to the fraction of particles between 200 and 1000  $\mu\text{m}$ , for the process for preparing three-layer microspheres, between 20 and 500  $\mu\text{m}$  for the process for preparing two-layer microspheres.

20 The feasibility of the process according to the invention is evaluated according to the ease with which the microspheres are obtained, the speed of production of a batch and the yield for each step.

25 Analysis of the batches includes particle size analysis of a sample of 100 g of spheres by the superimposed screens method (sample obtained from the total fraction of a batch), after which a morphological study of the microspheres obtained, relating to the overall appearance, sphericity, cohesion and uniformity of the particles, is carried out by examination with a binocular magnifying glass.

According to one variant of the invention, the two-layer or three-layer effervescent microspheres are manufactured by the mounting technique combined with a system for the tangential spraying of wetting liquid. The powder A and the powder B can be mounted successively on spheres  
5 containing oxytocin coated with water-soluble isolating agent, or on neutral spheres.

A further aspect of the invention is an effervescent formulation of oxytocin obtained or obtainable by any one of the processes of the invention  
10 mentioned above.

A further aspect of the invention provides an effervescent formulation of oxytocin for use in medicine.

15 A further aspect of the invention provides a pharmaceutical composition which comprises an effervescent formulation of oxytocin according to the invention and a pharmaceutically acceptable carrier.

A further aspect of the invention is a method of induction or augmentation  
20 of labour, or treatment or prevention of postpartum haemorrhage or treatment of missed abortion or facilitation of lactation comprising administering an effervescent formulation of oxytocin according to the invention and/or obtained or obtainable by a process according to the invention.

25

A further aspect of the invention is the use of an effervescent formulation of oxytocin according to the invention and/or obtained or obtainable by a process according to the invention in the manufacture of a medicament for the induction or augmentation of labour or treatment or prevention of



postpartum haemorrhage or treatment of missed abortion or facilitation of lactation.

Preferred embodiments of the invention are described in the following  
5 processes.

Process 1: Process for preparing multilayer effervescent microspheres containing an acidic substance, a basic substance, and a water-soluble isolating agent which upon dissolution in water leads, after almost  
10 immediate effervescence, to a solution or a homogeneous dispersion of oxytocin, wherein the acidic and basic substances contain or consist of oxytocin, which employs the method of rotary granulation in a fluidized air bed.

15 Process 2. Process for preparing microspheres defined in process 1, which employs the method of rotary granulation in a fluidized air bed combined with a system for spraying powder and a system for the tangential spraying of wetting liquid, which comprises two continuous steps, a first step of spheronization of microspheres using a powder A and a second step of  
20 spheronization of a powder B on the microspheres of powder A, one of the powders A and B being acidic and the other alkaline.

Process 3. Process according to process 2, wherein the powder A is introduced directly into the rotary granulation tank and then sprayed with a  
25 wetting liquid containing the water-soluble isolating agent, while the powder B and a wetting liquid containing the water-soluble isolating agent are simultaneously and respectively sprayed via the system for spraying powder and the system for the tangential spraying of liquid.

Process 4. Process according to process 3, wherein the microspheres obtained have an average particle size of between 20 and 500  $\mu\text{m}$ .

5 Process 5. Process for preparing microspheres as defined in process 1, which employs the method of rotary granulation in a fluidized air bed combined with a system for the tangential spraying of wetting liquid, which comprises three continuous steps, a first step of spheronization of microspheres using a powder A, a second step of spheronization of a water-soluble isolating agent on the microspheres of powder A, and then a third  
10 step of spheronization of a powder B on the microspheres A protected with a film of water-soluble isolating agent, one of the powders A and B being acidic and the other alkaline.

Process 6. Process according to process 5, wherein the powder A and the  
15 water-soluble isolating agent are sprayed with an alcoholic or aqueous-alcoholic solution.

Process 7. Process according to process 5, wherein the powder B contains the water-soluble isolating agent and is sprayed with an alcoholic or  
20 aqueous-alcoholic solution.

Process 8. Process according to process 5, wherein the powder B is sprayed with a wetting liquid containing the water-soluble isolating agent.

25 Process 9. Process according to process 5, wherein the microspheres obtained have an average particle size of between 200 and 1000  $\mu\text{m}$ .

Process 10. Process according to process 3, wherein the wetting liquid containing the water-soluble isolating agent is polyvinylpyrrolidone  
30 dissolved in an alcohol or an aqueous-alcoholic mixture, which is

polyvinylpyrrolidone dissolved to 4% by weight in ethanol at 60% by volume.

5 Process 11. Process according to process 2 or 5, wherein the powder of alkaline nature contains a sodium bicarbonate or another carbonate used in the preparation of effervescent forms, selected from lithium hydrogen carbonate, monosodium carbonate, lithium glycine carbonate, monopotassium carbonate, calcium carbonate, magnesium carbonate; and oxytocin.

10

Process 12. Process according to process 2 or 5, wherein the powder of acidic nature contains citric acid or ascorbic acid or, acetylleucine, and/or oxytocin.

15 Process 13. Process according to process 1, wherein the powder of alkaline nature also contain an edible diluent and; flavorings and sweeteners.

20 Process 14. Process according to process 2 or 5, wherein the microspheres obtained contain 5 to 75% of alkaline substance, 10 to 75% of acidic substance, 3 to 15% of water-soluble isolating agent, 5 to 50% of diluent, and 1 to 30% of flavorings and sweeteners.

Process 15. Process according to process 2 or 5, wherein the powder A is of alkaline nature and the powder B of acidic nature.

25

Process 16. Process according to process 2 or 5, wherein the powder A is of acidic nature and the powder B of alkaline nature.

Process 17. Process according to process 3 or 6, wherein the wetting liquid is sprayed by means of a nozzle 1.2 mm in diameter, at an average flow rate of between 10 and 30 g/min.

- 5 Process 18. Process according to process 2 or 5, wherein the air inlet temperature of the fluidized bed is between 55 and 65°C during spheronization steps, and between 75 and 85°C during drying phases associated with the spheronization steps.
- 10 Process 19. Process according to process 2 or 5, wherein the relative humidity of the microspheres obtained is between 1 and 2% at the rotary granulation tank outlet.

Process 20. Process for preparing microspheres as defined in process 1,  
15 which employs the mounting technique combined with a system for the tangential spraying of wetting liquid.

Process 21. Process according to process 20, wherein the powder A and the powder B are mounted successively on spheres containing oxytocin coated  
20 with water-soluble isolating agent, or on neutral spheres.

Process 22. Process according to process 12, wherein the powder of acidic nature also contains an edible diluent and flavorings and sweeteners.

- 25 The examples which follow illustrate the invention without limiting its scope.

The percentages are expressed on a weight basis.

**EXAMPLE 1**

Two-layer effervescent microspheres containing ascorbic acid (vitamin C)

- 5 Alkaline microspheres are prepared, on which is deposited the acidic substance (vitamin C).

The table below gives the details of the formulation used.

10	FORMULATION	COMPONENT	PERCENTAGE
	Powder A		
	Alkaline compound	Sodium bicarbonate	20%
	Diluent	Lactose	6%
15	Sweetener	Glucidex 6 .RTM.	6%
	Powder B		
	Acidic compound	Ascorbic acid	49.99994%
	Oxytocin		0.00006%
	Flavoring	Orange flavoring	1%
20	Sweeteners	Sodium saccharinate	0.3%
		Glucidex 6 .RTM.	6.35%
	Diluent	Lactose	6.35%

25

The wetting liquid used during the two successive rotary granulations is an aqueous-alcoholic PVP solution containing 4% PVP in ethanol at 60% by volume.

- 30 This mixture is sprayed at an average flow rate of 25 grams per minute.

In this formulation, the lactose is combined in equal part with Glucidex 60, although it is possible to use lactose alone.

The powder formulations A and B are prepared on batches of variable size of 1000 to 5000 g with, depending on the case, use of equipment from the company Glatt.

- 5 The effervescent spheres obtained have a fairly uniform appearance and a majority particle size of fractions between 200 and 500  $\mu\text{m}$ . The relative humidity is 1.6% at the rotary granulation tank outlet.

## EXAMPLE 2

10

Two-layer effervescent microspheres containing acetylleucine

Alkaline microspheres are prepared, on which is deposited the acidic substance (acetylleucine) under the same conditions as in Example 1.

15

The table below gives the details of the formulation used.

	FORMULATION	COMPONENT	PERCENTAGE
	Powder A		
20	Alkaline compound	Sodium bicarbonate	20%
	Diluent	Lactose	9.85%
	Powder B		
	Acidic compound	Acetylleucine	49.98%
25	Oxytocin		0.02%
	Flavoring	Orange flavoring	1%
	Sweetener	Sodium saccharinate	0.3%
	Diluent	Lactose	9.85%
30			

The particle size distribution of the batch is a majority for the fractions 25 to 500  $\mu\text{m}$ .

The relative humidity is 1.9% at the rotary granulation tank outlet.

According to the size of the batches ranging from 1000 to 10,000 g,  
5 apparatus GPCG 1 or GPCG 5 from the company Glatt with a rotor tank  
mounting [lacuna].

### EXAMPLE 3

10 Three-layer effervescent microspheres containing ascorbic acid (vitamin C)

Three-layer effervescent microspheres are manufactured, comprising an  
alkaline core isolated from the acidic substance, ascorbic acid, by means of  
a film of PVP.

15

	FORMULATION	COMPONENT	PERCENTAGE
	Powder A		
	Alkaline compound	Sodium bicarbonate	25%
20	Binder	PVP K30	1.316%
	Diluent	Lactose	7.950%
	Water-soluble isolating agent	PVP K30	6.958%
	Powder B		
25	Acidic compound	Ascorbic acid	49.998%
	Oxytocin		0.002%
	Flavoring	Orange flavoring	1%
	Sweeteners	Sodium saccharinate	0.2%
30		Citric acid	1%
	Diluent	Lactose	6.950%

The test is carried out in apparatus of GPCG1 type from the company Glatt,  
with the rotor tank mounting.

1460 g of ethanol at 60% by volume are sprayed in total during the three steps, at an average flow rate of 15 grams per minute.

- 5 The size of the final batch is 1000 g.

The working yield corresponding to the fraction of particles between 200 and 1000  $\mu\text{m}$  is 65%. The relative humidity is 1.5% at the tank outlet.

- 10 **Example 4: Induction or augmentation of labour with oxytocin**

A female patient presenting symptoms of delayed labour is treated with an effervescent formulation according to Example 1 which has been made into a tablet.

15

The patient is supplied with an effervescent formulation containing 340 ng of oxytocin in the form of a 500 mg tablet. The quantity of oxytocin used is dependent on the severity of the condition and the tolerance of the patient to oxytocin.

20

The patient places the tablet on the tongue. The tablet effervesces and delivers the oxytocin to the patient.

- 25 The oxytocin may be supplied to the patient in this manner every 30 minutes (with or without an escalating dose) until labour is progressing. In any event the skilled practitioner will be able to ascertain the amount and frequency of the doses to produce the required effect.



**Example 5: Induction or augmentation of labour with oxytocin**

A female patient presenting symptoms of delayed labour is treated with an effervescent formulation according to Example 2 which has been made into  
5 a tablet.

The patient is supplied with an effervescent formulation containing 11 µg of oxytocin in the form of a 50 mg tablet. The quantity of oxytocin used is dependent on the severity of the condition and the tolerance of the patient  
10 to oxytocin.

The patient places the tablet on the tongue. The tablet effervesces and delivers the oxytocin to the patient.

15 The oxytocin may be supplied to the patient in this manner every 30 minutes (with or without an escalating dose) until labour is progressing. In any event the skilled practitioner will be able to ascertain the amount and frequency of the doses to produce the required effect.

**CLAIMS**

1. An effervescent formulation comprising oxytocin.
- 5 2. An effervescent formulation according to Claim 1 comprising multilayer effervescent microspheres.
3. An effervescent formulation according to Claim 2 wherein the multilayer effervescent microspheres contain an acidic substance, a basic  
10 substance and water-soluble isolating agent.
4. An effervescent formulation according to Claim 3 wherein dissolution in water of the multilayer effervescent microspheres leads, after almost immediate effervescence, to a solution or a homogeneous dispersion  
15 of the oxytocin.
5. An effervescent formulation according to Claim 4 wherein the water-soluble isolating agent is dispersed in the entire bulk of each microsphere, the latter having a two-layer structure: a layer of acidic  
20 substance in which is dispersed the water-soluble isolating agent and a layer of alkaline substance in which is dispersed the water-soluble isolating agent.
6. An effervescent formulation according to Claim 4 wherein the  
25 water-soluble isolating agent is in the form of a thin film separating the acidic and alkaline substances such that each microsphere has a three-layer structure: a layer of acidic substance and a layer of alkaline substance separated by a layer of water-soluble isolating agent.

7. An effervescent formulation according to any of the preceding claims wherein the oxytocin is present in a unit dose amount of from 50 ng to 100 µg.
- 5 8. An effervescent formulation according to Claim 7 wherein the oxytocin is present in a unit dose amount of 340 ng to 11 µg.
9. An effervescent formulation according to any of the preceding claims wherein the formulation is presented in a tablet form.
- 10 10. An effervescent formulation according to Claims 1 to 8 wherein the formulation is presented in a powder form.
11. An effervescent formulation according to any of the preceding  
15 claims obtained or obtainable by the process of any one of Claims 14 to 20.
12. An effervescent formulation according to any one of the previous claims for use in medicine.
- 20 13. A pharmaceutical composition comprising an effervescent formulation according to any one of Claims 1 to 11 and a pharmaceutically acceptable carrier.
14. A process for making an effervescent formulation containing  
25 oxytocin.
15. A process according to Claim 14 wherein the effervescent formulation comprises multilayer effervescent microspheres containing an acidic substance, a basic substance, and a water-soluble isolating agent

which upon dissolution in water leads, after almost immediate effervescence, to a solution or a homogeneous dispersion of oxytocin.

16. A process according to Claim 15 wherein the acidic and/or basic  
5 substances contains or contain oxytocin.

17. A process according to Claim 16 which employs the method of rotary granulation in a fluidized air bed.

10 18. A process according to Claims 15 to 17 wherein basic substance also contains an edible dilutant and/or flavourings and/or sweeteners.

19. A process according to Claims 15 to 18 wherein the oxytocin is present in an amount to give from 50 ng to 100 µg in the final unit dosage  
15 form.

20. A process according to Claim 19 wherein the oxytocin is present in an amount to give from 340 ng to 11 µg in the final unit dosage form.

20 21. A process according to any one of Claims 14 to 20 further comprising preparing the microspheres into a tablet.

22. An effervescent formulation of oxytocin obtained or obtainable by the process of any one of Claims 14 to 21.

25

23. A method of induction or augmentation of labour or treating or preventing postpartum haemorrhage or treating missed abortion or facilitation of lactation comprising administering an effervescent formulation of oxytocin according to any one of Claims 1 to 11 and/or

obtained or obtainable by a process as defined in any one of Claims 14 to 21 and/or a pharmaceutical composition according to Claim 13.

24. Use of an effervescent formulation of oxytocin according to any one  
5 of Claims 1 to 11 and/or obtained or obtainable by a process as defined in  
any one of Claims 14 to 21 and/or a pharmaceutical composition according  
to Claim 13 in the manufacture of a medicament for the induction or  
augmentation of labour or treatment or prevention of postpartum  
haemorrhage or treatment of missed abortion or treatment of facilitation of  
10 lactation.

25. Any novel formulation, process, method, use or treatment of a  
disorder as herein disclosed.

**ABSTRACT****METHODS OF TREATMENT**

- 5 An effervescent formulation comprising oxytocin, preferably comprising multilayer effervescent microspheres containing an acidic substance, a basic substance and water-soluble isolating agent. An effervescent formulation comprising oxytocin wherein dissolution in water of the multilayer effervescent microspheres leads, after almost immediate
- 10 effervescence, to a solution or a homogeneous dispersion of the oxytocin. The formulation is used for the induction or augmentation of labour or treatment or prevention of postpartum haemorrhage or treatment of missed abortion or facilitation of lactation.

PCT Application  
**GB0304146**



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